

SUBCOOLED FLOW BOILING OF HFE-7000 UNDER ELECTRIC FIELD

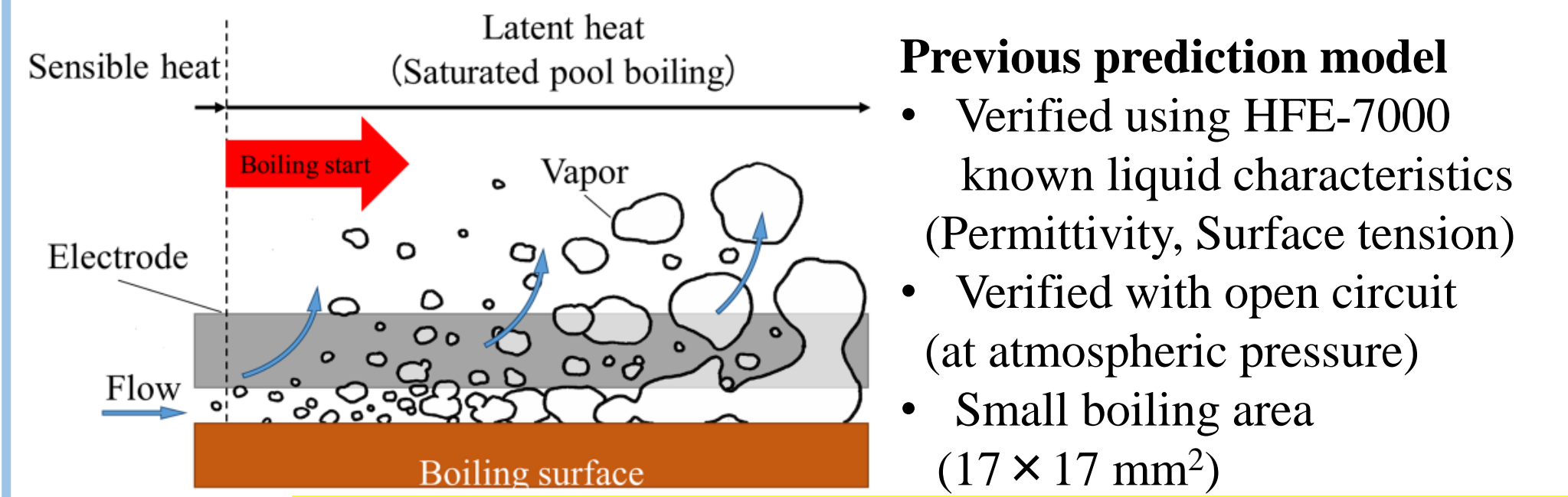
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Flow boiling

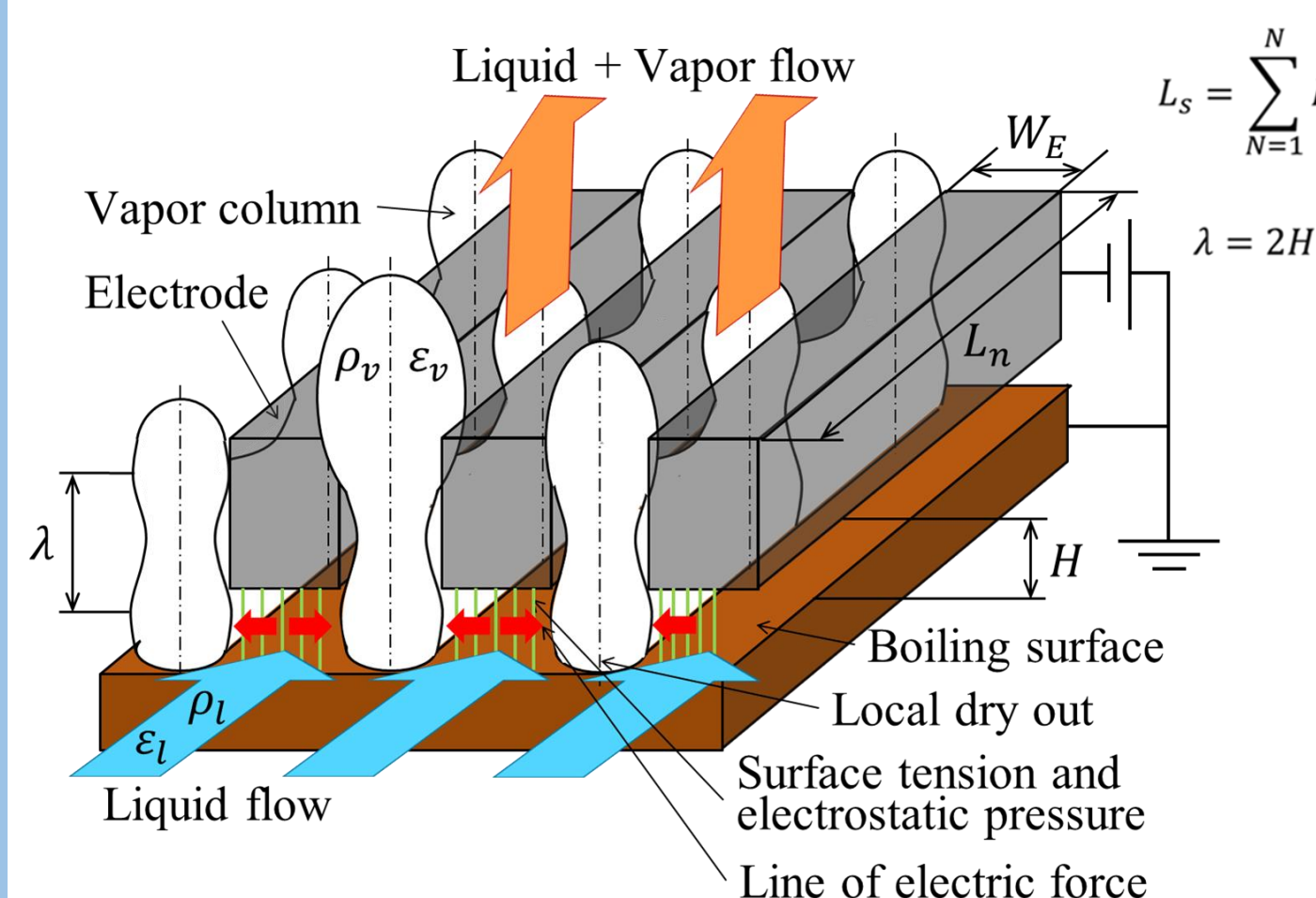
- Enhanced by electric field
- Increasing in CHF
20 W/cm² → 100 W/cm²
- Removing high heat flux at Low wall temperature
T_w < 60 °C

Prediction: no permittivity and surface tension of HCFO-1224yd (Low boiling point)

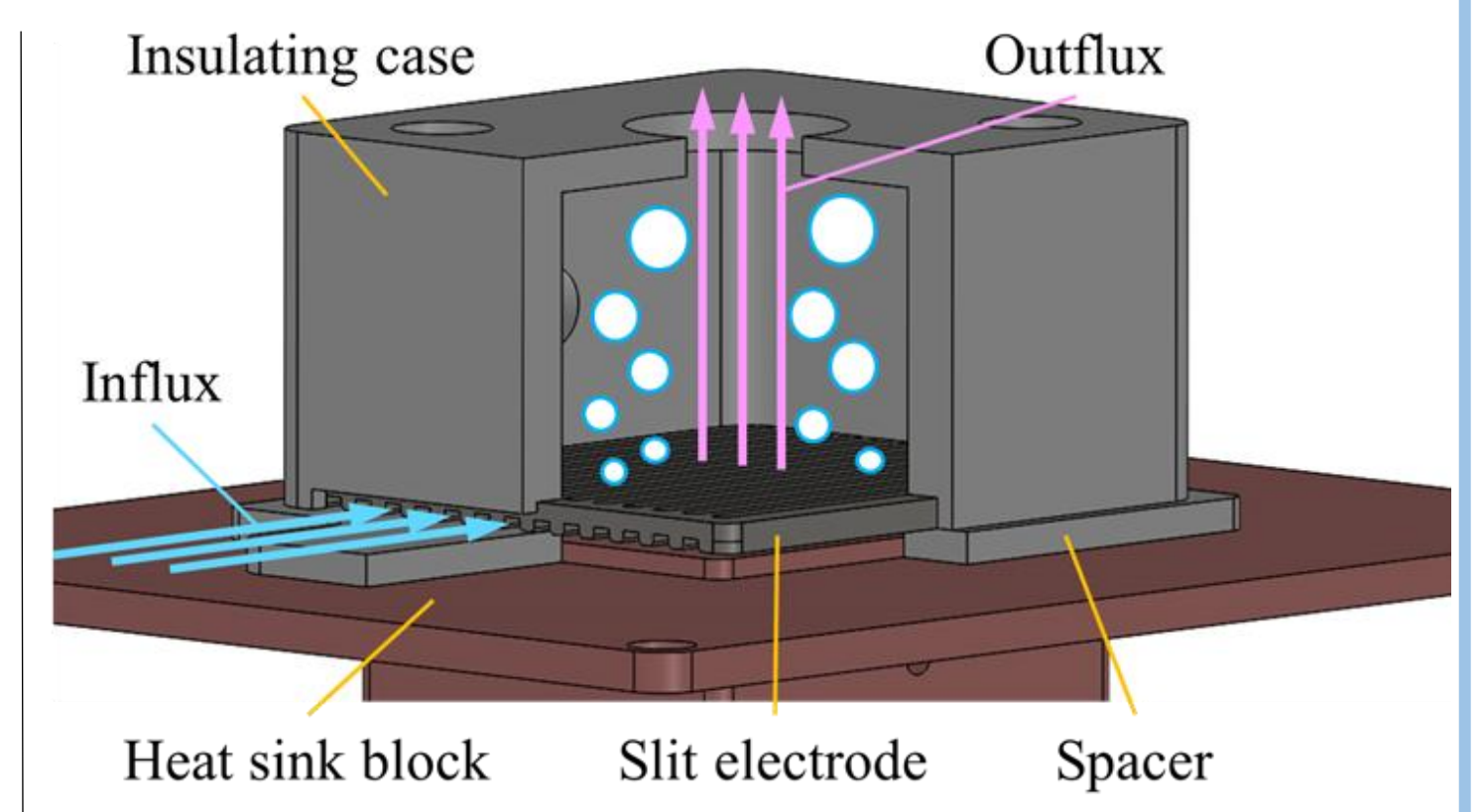


Aim of the study To predict CHF with previous prediction model using HFE-7000 at various system pressure (20, 70 128 kPaG) and a large boiling area (28 × 24.5 mm²).

Flow boiling model and CHF prediction



A : Boiling area [m²]
E_t : Electric field [V/m]
H : Distance between electrode and surface [m]
L : Latent heat [J/kg]
L_n : Slit length [m]
L_s : Total slits length [m]
ṁ : Mass flux [kg/s]
V : Voltage [V]
W_E : Electrode width [m]
ε_l : Liquid Permittivity [F/m]
ε_v : Vapor Permittivity [F/m]
λ : Wave length [m]
ρ_l : Liquid density [kg/m³]
ρ_v : Vapor density [kg/m³]
σ : Surface tension [N/m]



Latent heat (CHF prediction of saturated pool boiling),

Kano et al. (2022)

$$CHF_{ESP} = \frac{\pi \lambda}{48} L \rho_v \frac{L_s}{A} \left[\frac{\rho_l + \rho_v}{\rho_l \rho_v} \left\{ \frac{2\pi \sigma}{\lambda} + E_t^2 (\epsilon_l - \epsilon_v) \tanh \left(\frac{\pi W_E}{\lambda} \right) \right\} \right]^{\frac{1}{2}} \quad (1)$$

Sensible Heat flux and maximum heat flux

$$\Delta T_l = \frac{T_{in} - T_{out}}{2}$$

$$q_s = \frac{\dot{m} C_p \Delta T_l}{A}, \quad q_{s,max} = \frac{\dot{m} C_p \Delta T_{l,max}}{A}, \quad \Delta T_{l,max} = \frac{T_{in} - T_{sat}}{2} \quad (2)$$

CHF of subcooled flow boiling affected by contact angle

$$CHF_{sfb} = q_{s,max} + \left(C_A \frac{\cos \phi}{\sin^2 \phi} + C_B \frac{1}{\sin \phi} \right) CHF_{ESP} \quad (3)$$

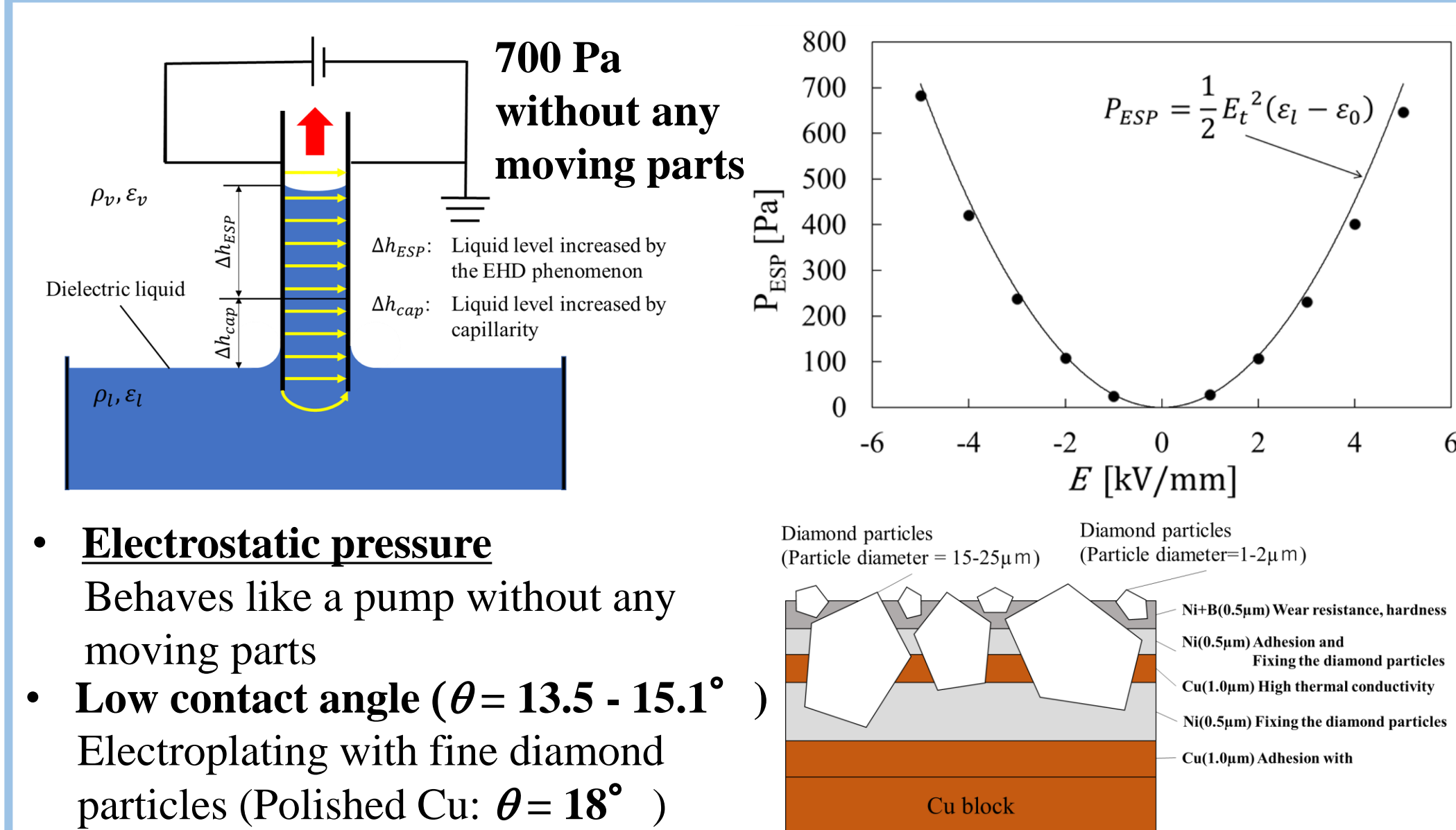
Upper limit of heat flux

$$CHF_{lim} = \frac{\dot{m} L}{A} + q_{s,max} \quad (4)$$

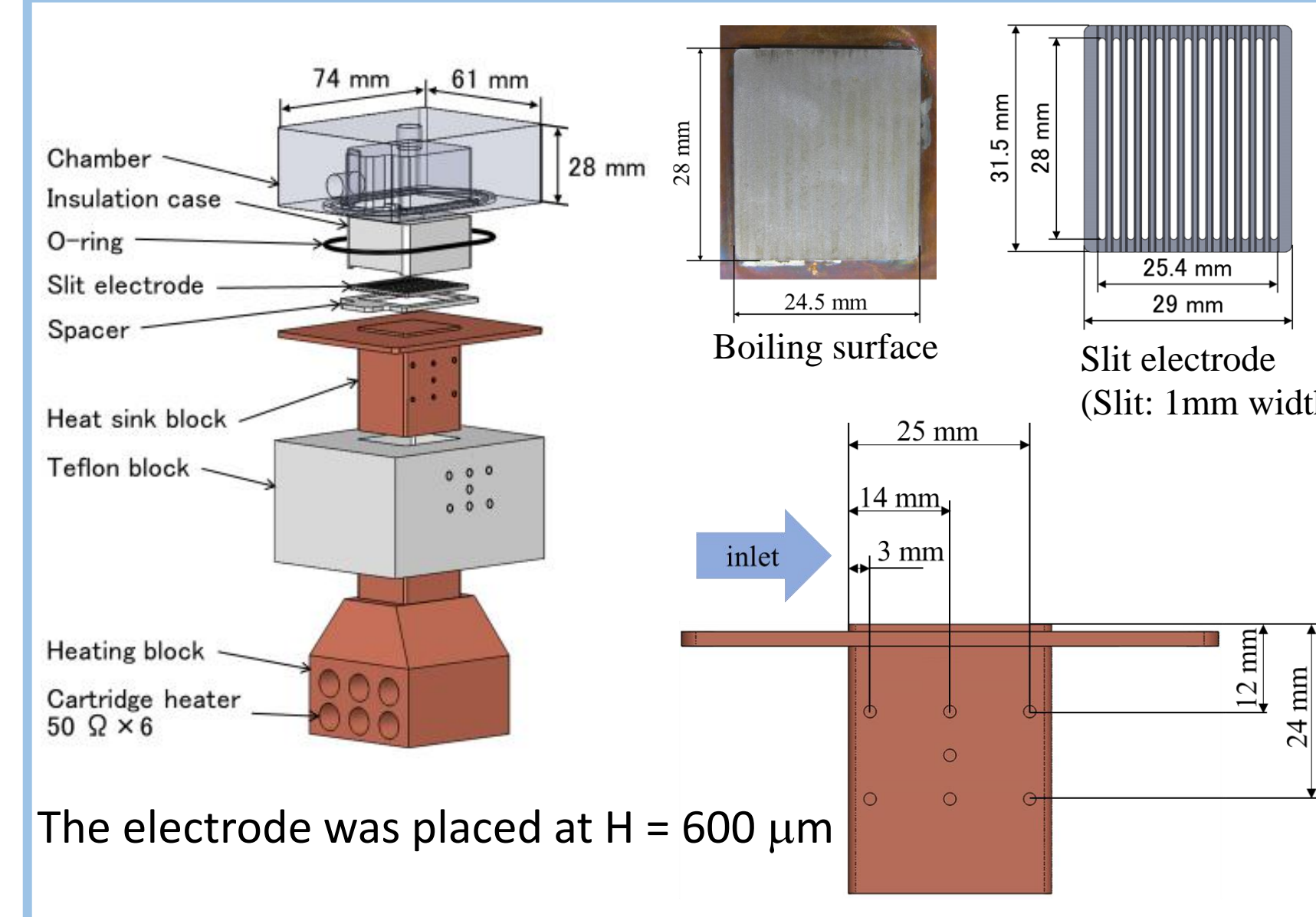
Vapor quality

$$\chi = \frac{(q - q_s) A}{\dot{m} L} \quad (5)$$

Enhancement techniques

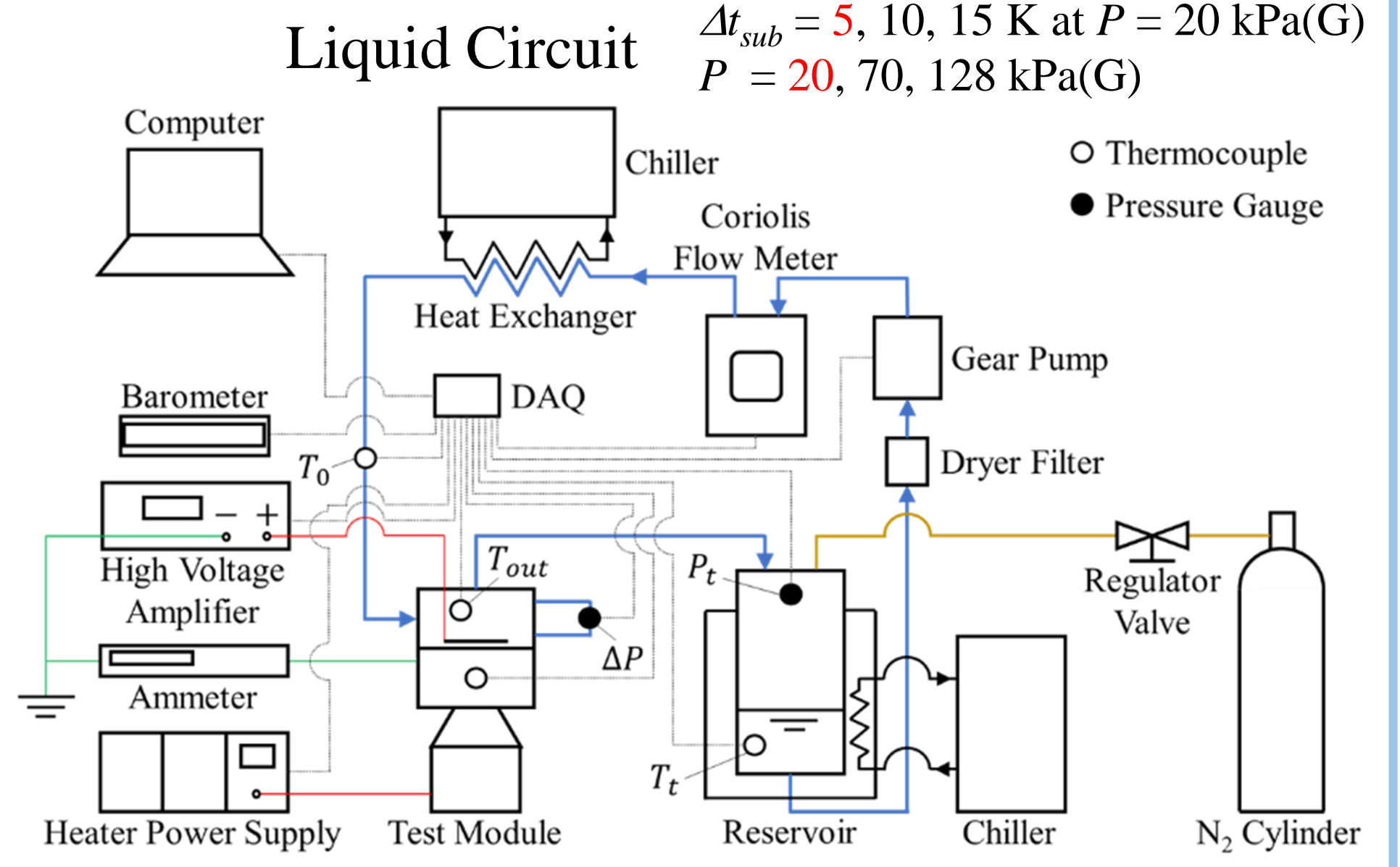


Experimental setup



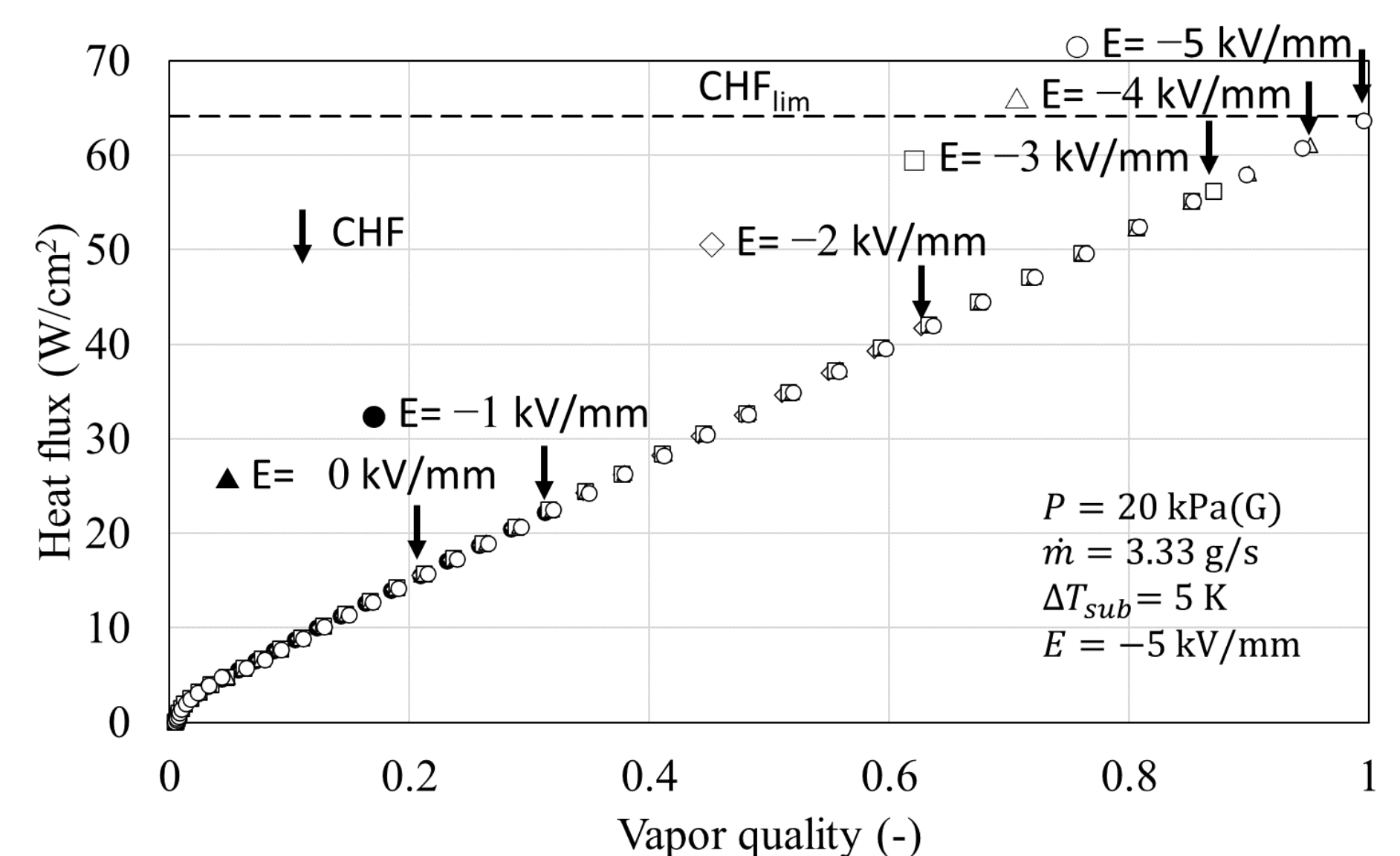
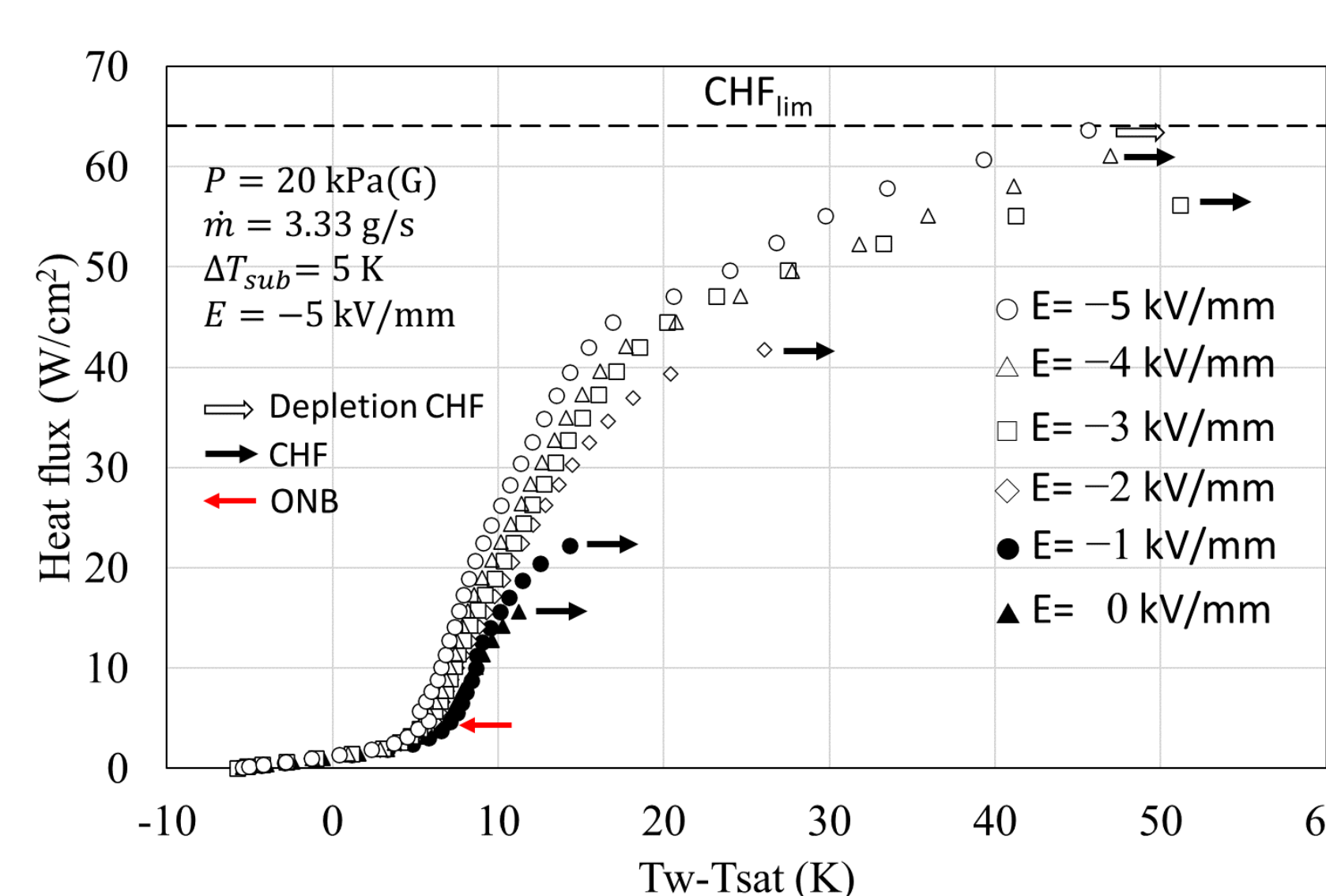
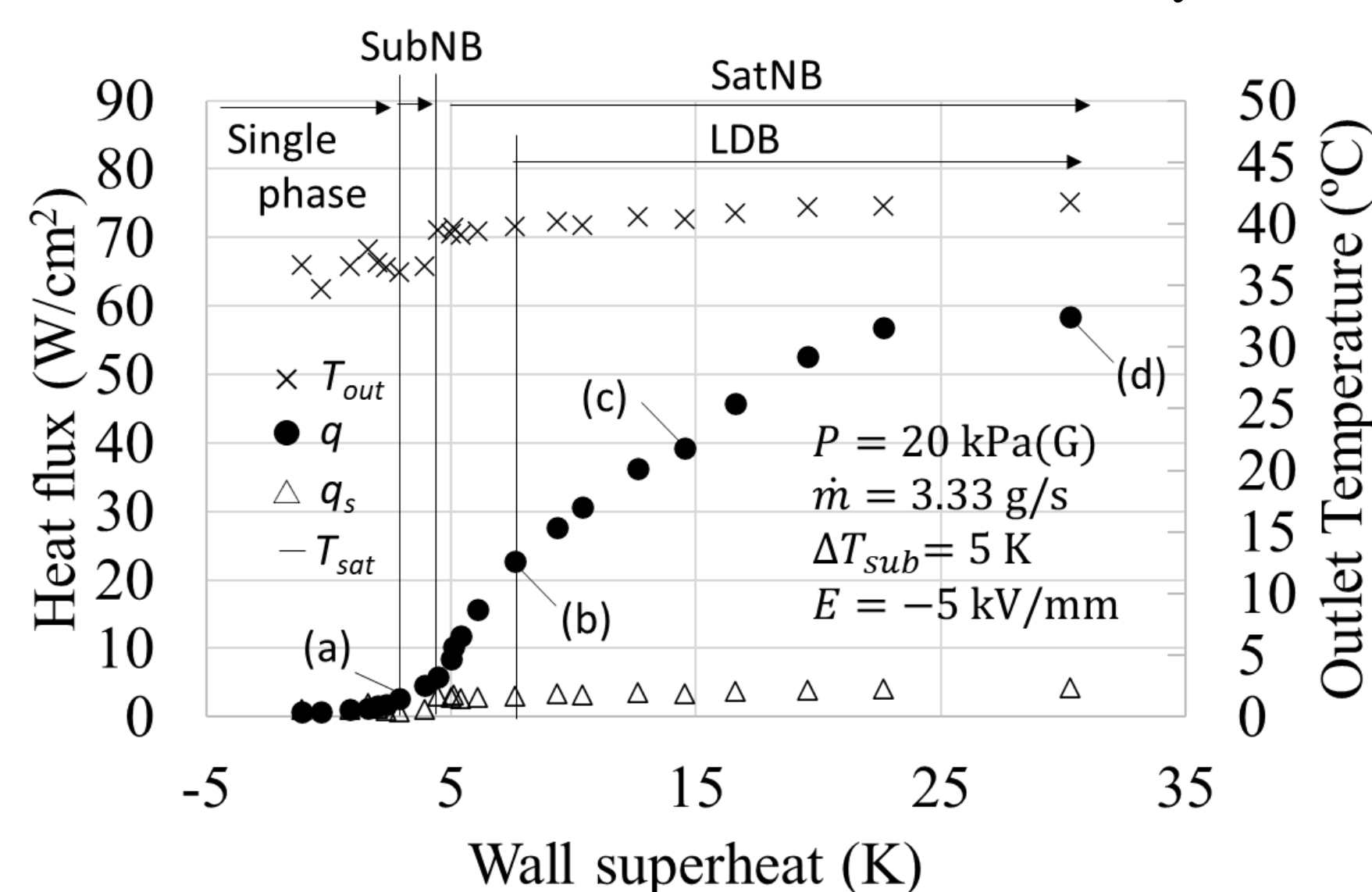
Refrigerant : HFE-7000
Boiling point at 1atm : 34 °C

Experimental condition
E = 0, -1, -2, -3, -4, -5 kV/mm
ṁ = 1.66, 3.33, 5.00 g/s
ΔT_{sub} = 5, 10, 15 K at P = 20 kPa(G)
P = 20, 70, 128 kPa(G)



Results

Sub : Subcooled
Sat : Saturated
NB : Nucleate Boiling
LDB : Local Dry-out Boiling



Boiling curve and Bubble behavior in MSC

- Single phase, Subcooled nucleate boiling, Saturated nucleate boiling regions
- Boiling starts in the subcooling condition
- Size of bubbles are not changed
- Heat flux suddenly increases due to latent heat
- Bubbles are coalesced and growth
- Local dry out occurred under the slits
- Almost inflow liquid is vaporized at the CHF

Effect of Electric field

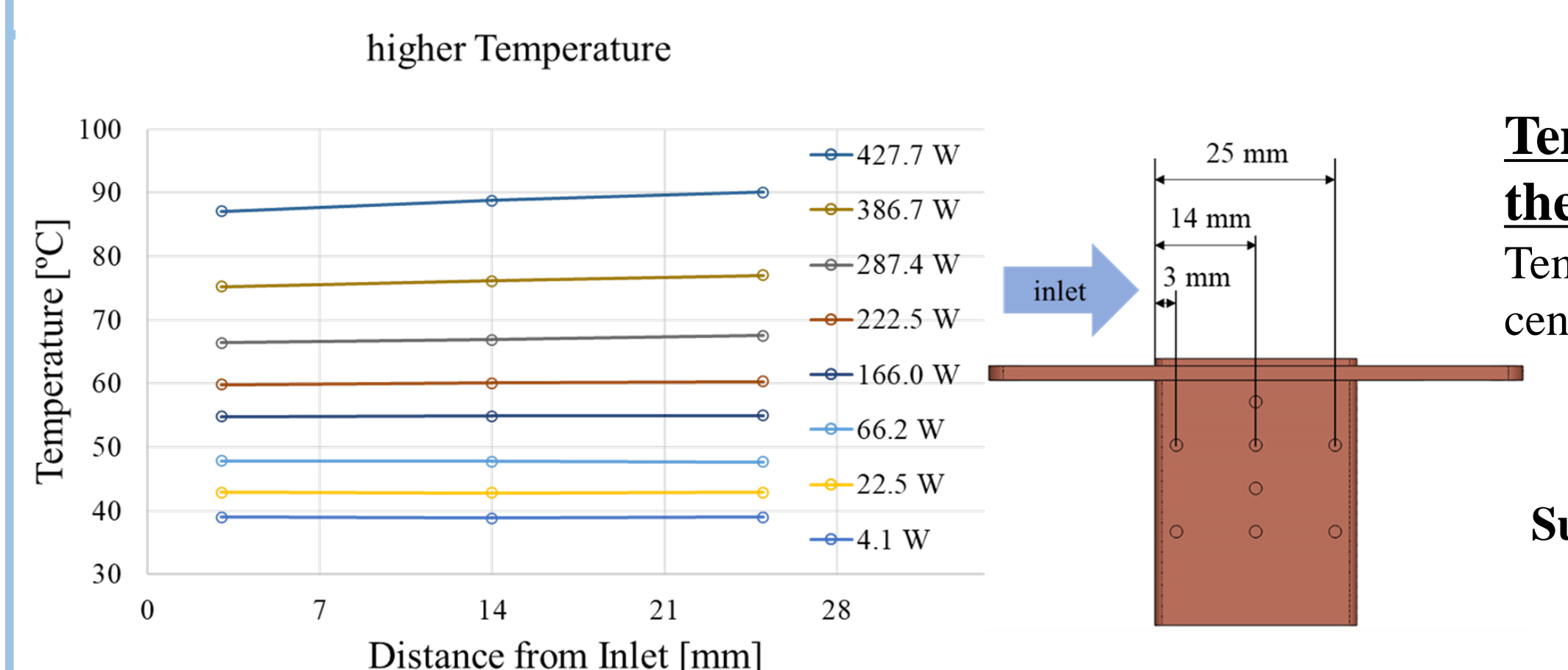
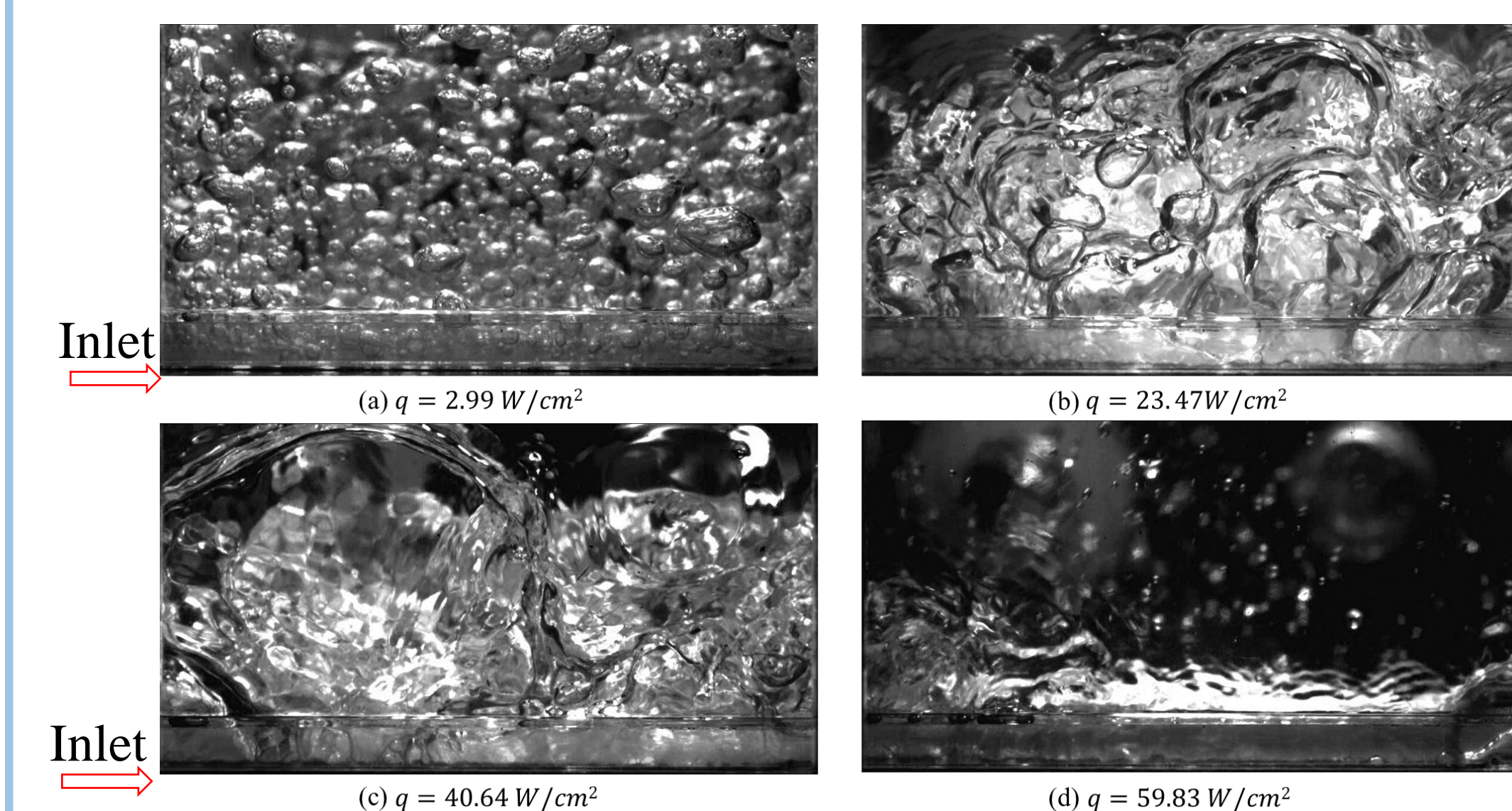
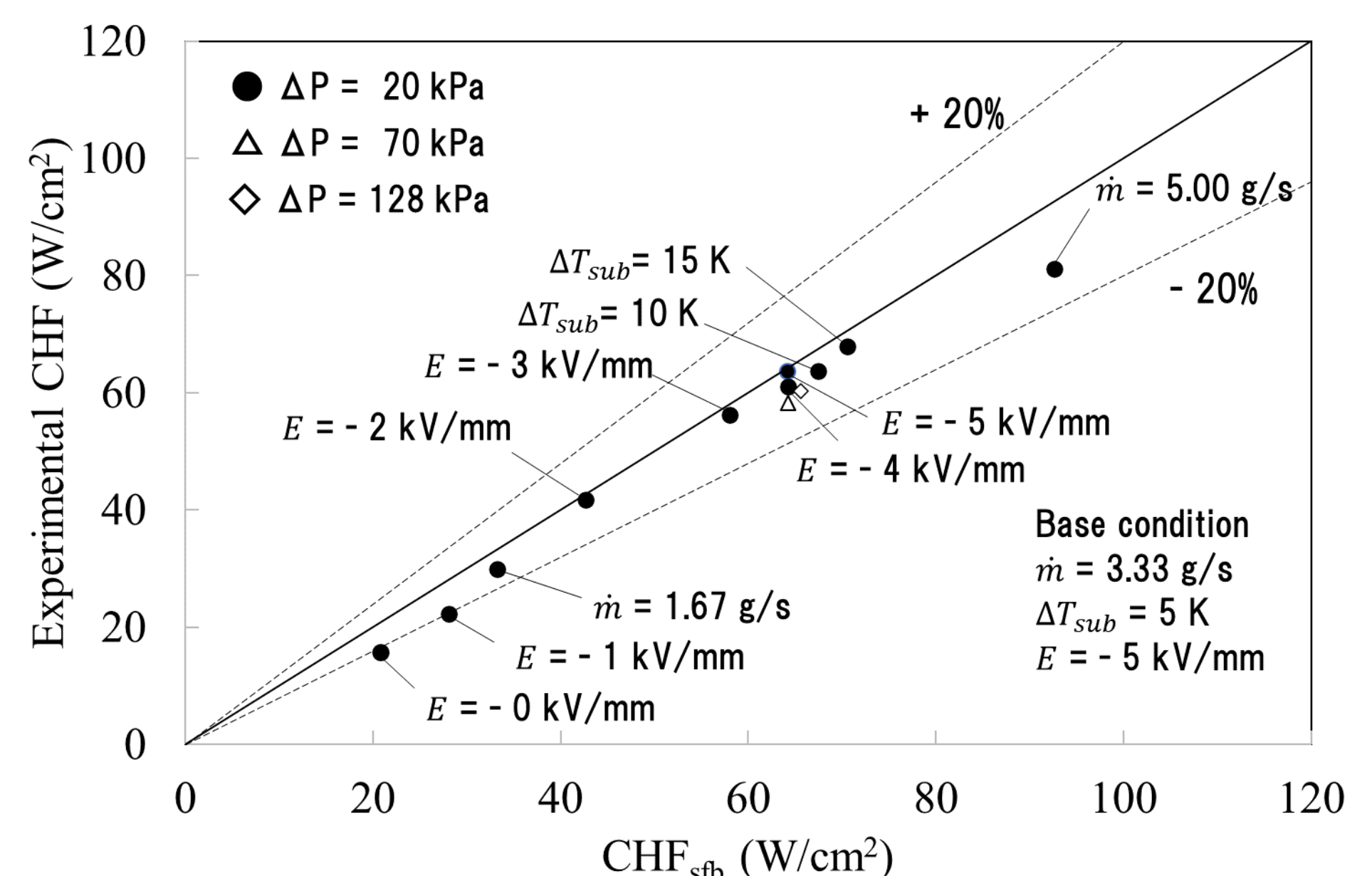
- 16 → 64 W/cm² (4 times greater)
- Heat flux reaches to a upper limit of heat flux at E = -5 kV/mm

Vapor quality

- Electric field effectively enhances the boiling until 100 % of inflow liquid is evaporated

Comparing with CHF prediction

- Effects of electric fields, additional system pressures, and mass flow rates were considered.
- Predicting CHF within ±20 %



Temperature distribution on the boiling surface

Temperature difference with the center is 1.9 %

Conclusion

Subcooled flow boiling CHF in closed and pressurized circuit was predicted within ±20 %

Future study

Heat transfer coefficient is very high, however, the thermal resistance (R_T = 0.06 K/W) is need to improve because of small boiling surface

We need to study the electric field enhancement technique over the additional boiling surface area like a plate-fin surface